



Contents

IN	FRODUC	TION		3						
GL	IIDANCE			3						
2.1	. Visc	osity		4						
	2.1.1	Dynamic	viscosity	4						
	2.1.2	Kinemati	nematic Viscosity							
	2.1.3	The Importance of Viscosity								
	2.1.3.		Lubrication							
	2.1.3.	2 Food	d and Drinks Industry	6						
	2.1.4	Kinemati	ic Viscosity – Temperature Relationship	6						
	2.1.4.									
	2.1.4.		> 100							
2.2	2 Visc									
	2.2.1	Capillary	Viscometers	9						
	2.2.2	Falling Sp	phere Viscometer	10						
	2.2.3	Rotation	al Viscometers	11						
	2.2.3.	1 Coue	ette Principle	12						
	2.2.3.		Searle Principle							
	2.2.3.	3 Serv	vo Devices	13						
	2.2.3.	4 Sprii	ng Devices	13						
	2.2.3.		ational Viscometer Equations							
	2.2.4		liscometars							
	2.2.4.	1 Sayb	oolt Viscometer	15						
	2.2.4.	2 Red	wood Viscometer	16						
2.3	8 Nev	vtonian ar	nd Non-Newtonian	17						
	2.3.1	Newtonia	an Fluids	17						
	2.3.2	Non-Nev	vtonian	17						
	2.3.2.	1 Dilat	tant Fluids	17						
	2.3.2.	2 Pseu	udoplastics	18						
	2.3.2.	3 Bing	sham Plastics	18						



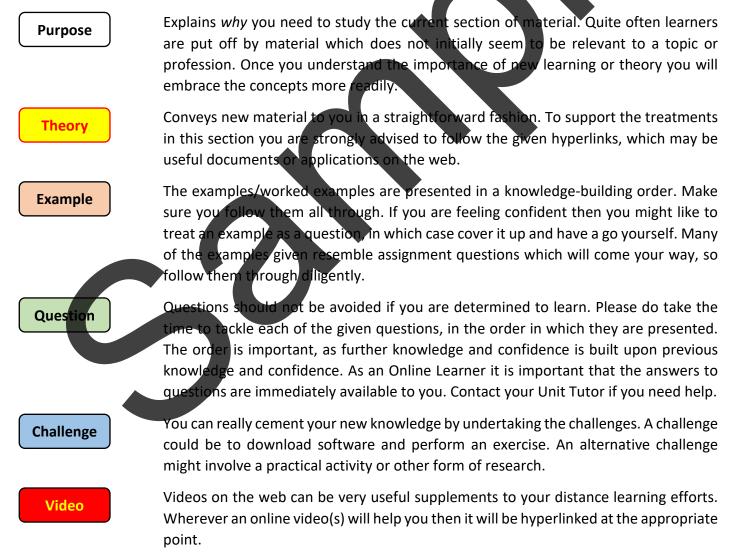
INTRODUCTION

Examine the operating principles and limitations of viscosity measuring devices

- Viscosity in fluids:
 - Dynamic and kinematic viscosity definitions.
 - Characteristics of Newtonian fluids.
 - Temperature effects on viscosity.
 - Classification of non-Newtonian fluids.
- Operating principles and limitations:
 - Operating principles of viscometers.
 - Converting results acquired from viscometers into viscosity values.

GUIDANCE

This document is prepared to break the unit material down into bite size chunks. You will see the learning outcomes above treated in their own sections. Therein you will encounter the following structures;





2.1 Viscosity

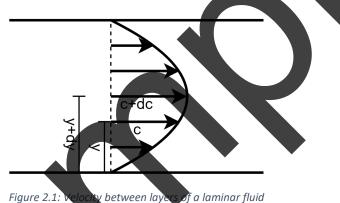
Viscosity is a fluid's resistance to deformation under shear stresses.

Viscosity is an important property of any fluid, as it also helps determine its behaviour and motion against solid boundaries (such as pipes, gears, sliding contacts etc.). The viscosity is determined by the intermolecular friction that is seen when one layer slides over the other. Or to put it simply, *viscosity is how runny the fluid is*. The higher the viscosity, the thicker, and less runny, the fluid is.

It is very important to note that viscosity is temperature dependent. When considering a shortlist of fluids to a given application, it is vital that the temperature of the system is also considered.

2.1.1 Dynamic Viscosity

Dynamic viscosity is the fluid's resistance to flow when an external force is applied. Dynamic viscosity can be thought of as the tangential force per unit area required to move one plane (layer) of fluid with respect to another. The velocity between layers of a laminar fluid moving in straight parallelyines for a Newtonian fluid can be seen in Fig.2.1.



The shear stress τ can be defined by Eq.2.1, where μ is the dynamic viscosity, c is the velocity of the fluid, y is the height from the surface. dc/dy is also known as the "shear rate".

$$\tau = \mu \frac{dc}{dy} \quad (2.1)$$

The SI units for dynamic viscosity is Pa · s, the values used are typically very low (e.g., the dynamic viscosity of water at $20^{\circ}C$ is 0.0010005 Pa · s. More commonly the units that are used are the Poise, P, or centipoise, cP, where $10 P = 1 Pa \cdot s$, therefore the dynamic viscosity of water at $20^{\circ}C$ is $0.010005 Pa \cdot s$.

2.1.2 Kinematic Viscosit

Kinematic viscosity is the fluid's resistive flow under its own weight (no external forces are applied, just gravity). The substance with the highest kinematic viscosity is tar pitch, which, despite appearing to be a solid and even shatters when it is hit with a hammer, is actually an incredibly viscous liquid, and will drip roughly once every ten years. An experiment widely recognised as the longest running in the University of Queensland, Australia, is analysing the drip of tar pitch and began in 1927. Since the drip occurs around once every ten years, it has never actually been seen; the last time it did drip, the webcam failed and missed it.

Kinematic viscosity, v, can be calculated using Eq.2.2, where ρ is the density of the fluid



2.1.4.1 VI < 100

In the majority of cases, and for examples within this unit we will only be looking at lubricants with a Viscosity Index (VI) of less than 100.

To calculate the VI, there are two pieces of information which must be known from the start; the Kinematic Viscosity (KV) at 40°C and at 100°C. The KV at 40°C is noted as U and the KV at 100°C is noted as Y in the following method.

If the value of KV at 100°C is between 2 cSt and 70 cSt then the table opposite is used to look up the corresponding values of 'L' and 'H', these letters merely signify some constants of viscosity at certain predefined temperatures. If the KV at 100°C is above the value of 70 cSt then the table is not used to find 'L' and 'H', but rather a separate formula is used, as follows:

$$L = 0.8353Y^2 + 14.67Y - 216$$

$$H = 0.1684Y^2 + 11.85Y - 97 \quad (2.4)$$

The viscosity index in either case is then calculated using Eq.2.5:

$$VI = 100 \frac{L - U}{L - H}$$

2.1.4.2 *VI* > 100

In the rare case that lubricants have a viscosity index greater than 100, then the following steps need to be taken.

- 1. Determine the kinematic viscosity of the sample at 40° C and 100° C
- 2. Determine the value of H
 - i. If $2 \text{ mm}^2/\text{s} < \text{Y} < 70 \text{ mm}^2/\text{s}$, the ATSM standards can be used; these values are shown in Table 2.1.
 - ii. If 70 mm²/s < Y, then *H* is calculated using Eq.2.4:
- 3. The viscosity index is therefore given as Eq.2.6:

Where:

$$VI = \frac{10^{N} - 1}{0.00715} + 100 \quad (2.6)$$

$$N = \frac{\log_{10} H - \log_{10} U}{\log_{10} Y} \quad (2.7)$$



Unit Workbook 2 - Level 4 ENG – U11 Fluid Mechanics © 2019 UniCourse Ltd. All Rights Reserved

Kinematic Viscosity at	,	,,	Kinematic Viscosity	,		Kinematic Viscosity	,		Kinematic Viscosity	,		Kinematic Viscosity	,		Kinematic Viscosity	,	
100°C, mm ² /s (cSt)	L	н	at 100°C, mm²/s (cSt)	L	н	at 100°C, mm ² /s (cSt)	L	н	at 100°C, mm ² /s (cSt)	L	н	at 100°C, mm²/s (cSt)	L	н	at 100°C, mm²/s (cSt)	L	н
2.00	7.994	6.394	7.00	78.00	48.57	12.0	201.9	108.0	17.0	369.4	180.2	24.0	683.9	301.8	42.5	1935	714.9
2.10	8.640 9.309	6.894 7.410	7.10	80.25 82.39	49.61 50.69	12.1	204.8 207.8	109.4 110.7	17.1	373.3 377.1	181.7 183.3	24.2 24.4	694.5 704.2	305.6 309.4	43.0 43.5	1978 2021	728.2 741.3
2.20	10.00	7.944	7.30	84.53	51.78	12.3	2107.0	112.0	17.2	381.0	184.9	24.6	714.9	313.0	43.5	2021	754.4
2.40	10.71	8.496	7.40	86.66	52.88	12.4	213.6	113.3	17.4	384.9	186.5	24.8	725.7	317.0	44.5	2108	767.6
2.50	11.45	9.063	7.50	88.85	53.98	12.5	216.6	114.7	17.5	388.9	188.1	25.0	736.5	320.9	45.0	2152	780.9
2.60	12.21	9.647	7.60	91.04 93.20	55.09 56.20	12.6 12.7	219.6 222.6	116.0 117.4	17.6	392.7 396.7	189.7	25.2 25.4	747.2	324.9	45.5	2197	794.5 808.2
2.70	13.00 13.80	10.25 10.87	7.80	93.20 95.43	56.20	12.7	222.6	117.4	17.8	400.7	191.3 192.9	25.4	758.2 769.3	332.7	46,5	2243 2288	821.9
2.90	14.63	11.50	7.90	97.72	58.45	12.9	228.8	120.1	17.9	404.6	194.6	25.8	779.7	336.7	\$7.0	2323	835.5
3.00	15.49	12.15	8.00	100.0	59.60	13.0	231.9	121.5	18.0	408.6	196.2	26.0	790.4	340.5	17.5	2380	849.2
3.10 3.20	16.36 17.26	12.82 13.51	8.10 8.20	102.3 104.6	60.74 61.89	13.1 13.2	235.0 238.1	122.9 124.2	18.1 18.2	412.6 416.7	197.8 199.4	26.2	801.6 812.8	344.4	48.0 48.5	2473	863.0 876.9
3.30	18.18	14.21	8.30	106.9	63.05	13.3	241.2	125.6	18.3	420.7	201.0	26.6	824.1	352.3	49.0	2521	890.9
3.40	19.12	14.93	8.40	109.2	64.18	13.4	244.3	127.0	18.4	424.9	202.6	26.8	835.5	356.1	49.5	2570	905.3
3.50	20.09	15.66	8.50	111.5	65.32	13.5	247.4	128.4	18.5	429.0	204.3	27.0	847.0	360.5	50.0	2618	919.6
3.60	21.08	16.42	8.60	113.9	66.48	13.6	250.6	129.8	18.6	433.2	205.9	27.2	857.5	364.6	50.5	2667	933.6
3.70 3.80	22.09 23.13	17.19 17.97	8.70 8.80	116.2 118.5	67.64 68.79	13.7 13.8	253.8 257.0	131.2 132.6	18.7 18.8	437.3	207.6	27.6	869.0 880.6	3/2.2	51.0 51.5	2717 2767	948.2 962.9
3.90	24.19	18.77	8.90	120.9	69.94	13.9	260.1	134.0	18.9	441.5 445.7	209.3	27.8	892.3	376.4	52.0	2817	977.5
4.00	25.32	19.56	9.00	123.3	71.10	14.0	263.3	135.4	19.0	449.9	212.7	28.0	904.1	380.6	52.5	2867	992.1
4.10	26.50	20.37	9.10	125.7	72.27	14.1	266.6	136.8	19.1	454.2	214.4	28.2	915.8	384.6	53.0	2918	1007
4.20	27.75	21.21	9.20	128.0	73.42	14.2	269.8	138.2	19.2	458.4	216.1	28.4	327.6	388.8	53.5	2969	1021
4.30	29.07	22.05	9.30	130.4	74.57	14.3	273.0	139/6	19.3	62.7	217.	28.6	938.6	393.0	54.0	3020	1036
4.40	30.48	22.92	9.40	132.8	75.73	14.4	276.3	141.0	19.4	467.0	219.4	28.8	951.2	396.6	54.5	3073	1051
4.50 4.60	31.96 33.52	23.81 24.71	9.50 9.60	135.3 137.7	76.91 78.08	14.5 14.6	279.5	142.4	19.5 19.6	471.3 475.7	221.1 222.8	29.0	963.4 975.4	401.1 405.3	55.0 55.5	3126 3180	1066 1082
4.70	35.13	25.63	9.70	140.1	79.27	14.7	289.4	145.3	9.7	479.7	224.5	29.4	987.1	409.5	56.0	3233	1097
4.80	36.79	26.57	9.80	142.7	80.46	14.8	289.7	146.8	19.8	483.9	226.2	29.6	998.9	413.5	56.5	3286	1112
4.90	38.50	27.53	9.90	145.2	81.67	14.5	293.0	148.2	19.9	488.6	227.7	29.8	1011	417.6	57.0	3340	1127
5.00	40.23	28.49	10.0	147.7	82.87	15.0	296.5	149.7	20.0	493.2	229.5	30.0	1023	421.7	57.5	3396	1143
5.10	41.99	29.46	10.1	150.3	84.08	15.1	300.0	51.2	20.2	501.5	233.0	30.5	1055	432.4	58.0	3452	1159
5.20 5.30	43.76 45.53	30.43 31.40	10.2	152.9 155.4	25.30	15.2	303.4 306.9	152.6	20.4 20.6	510.8 519.9	236.4 240.1	31.0 31.5	1086 1119	443.2 454.0	58.5 59.0	3507 3563	1175 1190
5.40	47.31	32.37	10.3	158.0	1.72	15.4	310.3	155.6	20.8	528.8	243.5	32.0	1151	464.9	59.5	3619	1206
5.50	49.09	33.34	10.5	160.6	88.95	15.5	313.9	157.0	21.0	538.4	247.1	32.5	1184	475.9	60.0	3676	1222
5.60	50.87	34.32	19.6	163.2	30.19	15.6	317.5	158.6	21.2	547.5	250.7	33.0	1217	487.0	60.5	3734	1238
5.70	52.64	35.29	10.7	165.8	91.40	15.7	321.1	160.1	21.4	556.7	254.2	33.5	1251	498.1	61.0	3792	1254
5.80 5.90	54.42 Fa.20	36.26	10.8	168.5 171.2		15.8 15.9	24.6	161.6 163.1	21.6 21.8	566.4 575.6	257.8 261.5	34.0 34.5	1286 1321	509.6 521.1	61.5 62.0	3850 3908	1270 1286
						TO BE											
6.00	57.97 59.74	38.19 39.17	11.0	173.9		10.0	331.9	164.6	22.0	585.2		35.0	1356	532.5	62.5	3966	1303
6.10 6.20	59.74	40.15	12	176. 179.4	96.45 97.71	16.1 16.2	335.5 339.2	166.1 167.7	22.2	595.0 604.3	268.6 272.3	35.5 36.0	1391 1427	544.0 555.6	63.0 63.5	4026 4087	1319 1336
6.30	63.32		11.3	182.1	98.97	16.3	342.9	169.2	22.6		275.8	36.5	1464	567.1	64.0	4147	1352
6.40	65.18	42.14	11.4	184.9	100.2	16.4	346.6	170.7	22.8	624.1	279.6	37.0	1501	579.3	64.5	4207	1369
6.50	67.12	43.18	11.5	187.6	101.5	16.5	350.3	172.3	23.0	633.6		37.5	1538	591.3	65.0	4268	1386
6.60		44.24	11.6	190.4	102.8	16.6		173.8	23.2	643.4	286.8	38.0	1575	603.1	65.5	4329	1402
6.70	71.29		11.7	193.3	104.1	16.7		175.4	23.4	653.8		38.5	1613	615.0	66.0	4392	1419
6.80 6.90		46.44 47.51	11.8 11.9	196.2 199.0	105.4 106.7	16.8 16.9	361.7 365.6	177.0 178.6	23.6 23.8	663.3 673.7		39.0 39.5	1651 1691	627.1 639.2	66.5 67.0	4455 4517	1436 1454
												40.0	1730	651.8	67.5	4580	1471
												40.5	1770	664.2	68.0	4645	1488
												41.0	1810	676.6	68.5 69.0	4709	1506
												41.5	1851 1892	689.1 701.9	69.0	4773 4839	1523 1541
															70.0	4905	1558

Table 2.1: ATSM values for L and H for the sample oil of viscosity between $2 - 70 mm^2/s$

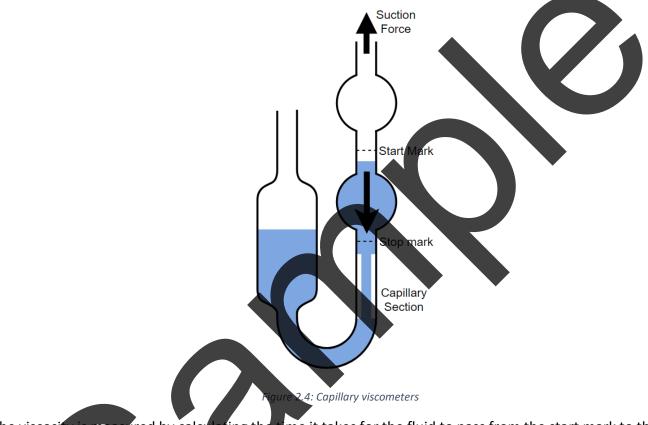


2.2 Viscometers

Viscometers are used to measure the viscosity of the fluid, and there are several types that exist.

2.2.1 Capillary Viscometers

Otherwise known as u-tube or glass viscometers, shown in Fig.2.4. These are the most common viscometers, they are cheap and relatively easy to use, and best suited for transparent or translucent liquids. The method is simple, use suction to bring the fluid up to the start mark (or ideally further past it). Once the suction is removed, the fluid will start to flow downwards.



The viscosity is measured by calculating the time it takes for the fluid to pass from the start mark to the stop mark. The equation used to calculate the kinematic viscosity of the fluid is given by Eq.2.8, where t is the time taken for the fluid to pass between the two marks, and K is the capillary constant of the viscometer, which is calibrated by measuring a reference liquid of known viscosity.

$$v = K_c \cdot t$$
 (2.8)



tar pitch), and so rotational viscometers employ a motor to add a rotational driving force. Rotational viscometers can apply two different principles to calculate viscosity:

- Couette Principle
- Searle Principle

Viscometers also measure torque using two different systems.

- Servo systems
- Spring systems

2.2.3.1 Couette Principle

The Couette principle relies on a bob to be suspended in a container filled with the test fluid. In this case, the driving force is acting on the container itself, meaning that the bob is the stationary frame of reference in the system (shown in Fig.2.6). This design avoids any problems with turbulent flow, but it is rarely used in commercial applications as it can be difficult to ensure that the container is well insulated and sealed in the rotating cup.

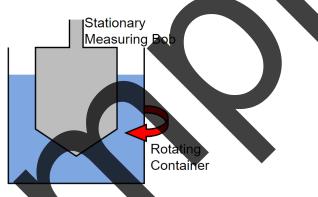


Figure 2.6: Couette principle rotational viscometer

2.2.3.2 The Searle Principle

The Searle principle holds the container stationary, and instead spins the measuring bob (as can be seen in Fig.2.7). In this case, the viscosity is proportional to the motor torque that is required for turning the bob against the resistive viscous forces of the fluid. These are much more common viscometers; however, the measuring bob must be kept at a low enough velocity to ensure that the flow in the container does not become turbulent.

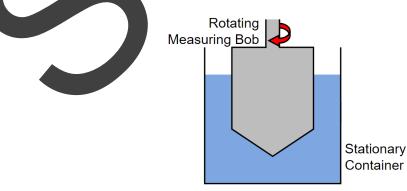


Figure 2.7: Searle principle rotational viscometer



2.2.4 Orifice Viscometers

Orifice viscometers are used in the oil industry because of their simplicity and ease of use. The system consists of a reservoir, an orifice and a receiver. The method is simple; the sample fluid is poured into the reservoir, which is temperature controlled in a water bath. Once the sample fluid has reached the desired temperature (that of the water bath), a valve at the base of the reservoir is opened and the time taken for a specific amount of sample fluid to flow out of the orifice is measured. While the industry has several types of orifice viscometers, this workbook will only look at the Saybolt and Redwood viscometers.

Other orifice viscometers include:

- Engler viscometers
- Ford viscosity cup viscometer
- Shell viscosity cup viscometer
- Zahn cup viscometer

2.2.4.1 Saybolt Viscometer



A schematic of the Saybolt viscometer is shown in Fig.2.9. A practical system would most likely have a thermometer in both the water bath and the sample fluid reservoir, as a sure way to make sure that the temperature is controlled - something that isn't accurately controlled in comparison to the capillary, falling sphere or rotational viscometers. Since this system analyses the flow rate of the fluid with only a force due to gravity acting on the fluid, the Saybolt viscometer calculates the kinematic viscosity.

The Saybolt viscometer gives its own unit of viscosity, "Saybolt seconds". This is the time it takes for 60 ml to pour into the receiver, whilst it is not as scientific as $Pa \cdot s$, it is a valid measurement of viscosity. Most standards analyse the viscosity in Saybolt seconds at $100^{\circ}F$. A reasonable estimate for a given temperature can be found using Eq.2.13, where v_T is the Saybolt kinematic viscosity at the desired temperature, T is the desired temperature, and $v_{100^{\circ}F}$ is the Saybolt kinematic viscosity at $100^{\circ}F$.

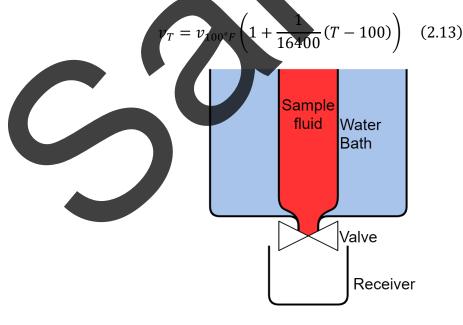


Figure 2.9: Saybolt viscometer



2.2.4.2 Redwood Viscometer

A schematic of the Redwood viscometer is shown in Fig.2.10 below. It bears a striking resemblance to the Saybolt viscometer, with the exception being that the valve is now a ball valve. Once the desired temperature for the sample has been reached, the ball is pulled out of the orifice and the sample fluid flows into the receiver. Again, this viscometer analyses the kinematic viscosity.

The Redwood viscometer also has its own units for viscosity, "redwood seconds". This is the time it takes for 50 ml to pour into the receiver.

