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INTRODUCTION

Apply the Steady Flow Energy Equation to plant equipment:

- Conventions used when describing the behaviour of heat and work.
- The Non-Flow Energy Equation as it applies to closed systems.
- Assumptions, applications and examples of practical systems.
- Steady Flow Energy Equation as applied to open systems.
- Assumptions made about the conditions around, energy transfer and the calculations for specific plant equipment e.g. boilers, super-heaters, turbines, pumps and condensers.

GUIDANCE

This document is prepared to break the unit material down into bite size chunks. You will see the learning outcomes above treated in their own sections. Therein you will encounter the following structures;





2.1 Energy equations

2.1.1 Heat and Work

Theory

When calculating heat and work, it's important to know the convention for calculations. Consider Eq.2.1 below.

$$Q - W = U_2 - U_1$$
 (Eq.2.1)

This is the equation used in a closed system, typically the compression or expansion stroke of a piston. The convention for energy transfer is:

- if heat is transferred from the surroundings into the system, then Q is **positive**
- if heat is released from the system into the surroundings, then Q is **negative**
- If external work is done **by** the fluid or engine, then W is **positive**
- if external work is done **on** the fluid or engine, then W is **negative**

Example 1

Calculate the work of an engine for one stroke if the heat transferred out of the system is 300 kJ/kg and the internal energy has decreased by 900 kJ/kg. State whether work is done on or by the fluid.

$$Q - W = U_2 - U_1$$

Heat is transferred out of the system, so Q is **negative**, and $U_2 - U_1$ is also **negative** since there is a decrease in internal energy.

$$-300 - W = -900$$
$$-W = -900 + 300$$
$$-W = -600$$
$$W = 600 \, kJ/kg$$

The work is positive, therefore work is done by the fluid



2.2 Closed System

2.2.1 Non-Flow Energy Equation

Theory

The Non-Flow Energy Equation is given as Eq.2.1. No flow means that there is no kinetic or potential energy. The assumptions when calculating a closed system are:

- The fluid is compressible
- The system is insulated meaning that heat is not lost to the environment over time
- The fluid is a "perfect" gas the implication of this term will be discussed in Section 2.1.3

2.2.2 Applying the Non-Flow Energy Equation

Theory

Most problems are simplified into defining one aspect of the system as constant. Table.2.1 shows the equations used to calculate work, internal energy and heat for the Non-Flow

Energy Equation. Using the equations defined in workbook 1 will help find the temperature, pressure and volume.

The term C_v seen in the table is the specific heat capacity of the fluid at constant volume. There is also the specific heat capacity at constant pressure, C_p . The ratio $C_v/C_p = \gamma$ is used in the calculations mentioned in workbook 1. The specific heat capacities will change with temperature, and so the assumption of "a perfect gas" is used, which means that C_v , C_p and γ are constant at all temperatures.

Process	P,V,T relationship	W	Δυ	Q
Isobaric constant pressure	$\frac{V_1}{T_1} = \frac{V_2}{T_2}$	$P(V_2 - V_1)$	$mc_p(T_2-T_1)$	$mc_p(T_2-T_1)$
Isochoric constant volume	$\frac{P_1}{T_1} = \frac{P_2}{T_2}$	0	$mc_v(T_2-T_1)$	$Q = U_2 - U_1$ $Q = mc_v(T_2 - T_1)$
Isothermal constant temperature	$\begin{aligned} \mathbf{T} &= c\\ P_1 V_1 &= P_2 V_2 \end{aligned}$	$P_1 V_1 ln\left(\frac{V_2}{V_1}\right)$	0	$Q = W$ $Q = P_1 V_1 ln\left(\frac{V_2}{V_1}\right)$
Polytropic reversible heat and work transfer	$PV^{n} = constant$ $\frac{T_{2}}{T_{1}} = \left(\frac{V_{1}}{V_{2}}\right)^{n-1}$ $\frac{P_{2}}{P_{1}} = \left(\frac{T_{2}}{T_{1}}\right)^{\frac{n}{n-1}}$	$\frac{P_1V_1 - P_2V_2}{n-1}$	$mc_v(T_2-T_1)$	$Q = W + U_2 - U_1$
Adiabatic no heat transfer	$PV^{\gamma} = constant$ $\frac{T_2}{T_1} = \left(\frac{V_1}{V_2}\right)^{\gamma-1}$ $\frac{P_2}{P_1} = \left(\frac{T_2}{T_1}\right)^{\frac{\gamma}{\gamma-1}}$	$\frac{P_1V_1 - P_2V_2}{\gamma - 1}$	$mc_v(T_2-T_1)$	0

Table.2.1: Equations used to calculate heat, work and internal energy for a closed system



Example 2

A closed system has a four-stage process. The working fluid's original state is 293K at 0.1MPa. The system then shrinks from $0.3m^3$ down to $0.15m^3$ through isentropic compression. The fluid then undergoes isobaric heating and expands to $0.18m^3$. The system then undergoes isentropic expansion back to $0.3m^3$, before isochoric cooling to its original state. Calculate:

- a) the work, heat and internal energy change of each stage.
- b) the overall work, heat and internal energy change of the system.
- c) and calculate the overall efficiency of the system.

Assume the working fluid is air acting as a perfect gas, with;

$$C_V = 0.718 \, kJ \cdot kg^{-1} \cdot K^{-1}$$

$$C_p = 1.00 \ kJ \cdot kg^{-1} \cdot K^{-1}$$

$$R = 0.287$$

 $\gamma = 1.4.$

Answer:

Check your answers with the excellent online OMINICALCULATOR which is very useful for confirming your solutions on many of your course modules.

a) First, we draw the P-V diagram.



Stage 1-2: Isentropic Compression.

Isentropic expansion means no heat transfer (i.e. adiabatic). Therefore;

 $PV^{\gamma} = constant$

v

$$\therefore \quad P_1 V_1^{\gamma} = P_2 V_2^{\gamma} \quad \therefore \quad \left(\frac{V_2}{V_1}\right)^{\gamma} = \frac{P_1}{P_2} \quad \therefore \quad P_2 = \frac{P_1}{\left(\frac{V_2}{V_1}\right)^{\gamma}} = \frac{0.1 \times 10^6}{\left(\frac{0.15}{0.3}\right)^{1.4}} = 263.9 \ kPa$$

